

Simulation of Turbulent Disperse Bubbly Flows

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Introduction

- High technical relevance of bubbly flows
 - Boiling water reactors (nuclear industry)
 - Air lift pumps (oil industry)
 - Chemical reactors (process industry)
- Largely empirical design to date due to complex flow physics
- Direct Numerical Simulation (DNS), resolving the full spectrum of turbulent scales, now possible for reduced-complexity configurations at moderate Reynolds number
- Computationally less expensive **Large Eddy Simulation (LES)** applicable to technically relevant cases
- **Goal:** Development of LES sub-grid scale closures for two-phase flows
- Working program
 - Creation of DNS database
 - Sub-grid term order of magnitude analysis
 - A-priori analysis of several existing and new LES models
 - A-posteriori assessment of most promising approaches
 - Comparison with experiment (Haase et al. [1])

Computational Fluid Dynamics (CFD)

- Parallel Robust Interface Simulator (PARIS) finite-volume solver (Zaleski et al. [2])
- Unsteady incompressible Navier-Stokes equations
- One-fluid formulation (density and viscosity jump at interface)
- Geometrical Volume-Of-Fluid (VOF) method with Piece-wise Linear Interface Calculation (PLIC) for interface propagation
- Curvature calculation by height function method
- Third-order QUICK convection scheme and time integration by second-order explicit Heun scheme
- Digital filter method for synthetic inflow turbulence (Klein et al. [3])
- SuperMUC high performance cluster

LES methodology

- Favre-filtered governing equations (Labourasse et al. [4])

$$\frac{\partial \bar{\rho}}{\partial t} + \nabla \cdot (\bar{\rho} \tilde{\mathbf{u}}) = 0$$

$$\frac{\partial \bar{\rho} \tilde{\mathbf{u}}}{\partial t} + \nabla \cdot (\bar{\rho} \tilde{\mathbf{u}} \otimes \tilde{\mathbf{u}} + \bar{p} \mathbf{I} - \bar{\mu} \tilde{\mathbf{S}}) - \bar{\rho} \mathbf{g} - \sigma \bar{\mathbf{n}} \bar{\kappa} \delta_S = -\nabla \cdot (\tau_{\rho uu} + \tau_{\mu S}) + \tau_{nn}$$

$$\frac{\partial \bar{\alpha}}{\partial t} + \tilde{\mathbf{u}} \cdot \nabla \bar{\alpha} = \tau_{u\alpha}$$

- Sub-grid scale contributions which need to be modeled

$$\tau_{\rho uu} = \overline{\rho \mathbf{u} \otimes \mathbf{u}} - \bar{\rho} \tilde{\mathbf{u}} \otimes \tilde{\mathbf{u}}$$

$$\tau_{\mu S} = \overline{\mu \mathbf{S}} - \bar{\mu} \tilde{\mathbf{S}}$$

$$\tau_{nn} = \overline{\sigma \mathbf{n} \kappa \delta_S} - \sigma \bar{\mathbf{n}} \bar{\kappa} \delta_S$$

$$\tau_{u\alpha} = \overline{\tilde{\mathbf{u}} \cdot \nabla \alpha} - \bar{\mathbf{u}} \cdot \nabla \alpha$$

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Bubble dynamics and bubble-induced turbulence

- Three sources of fluctuation/unsteadiness
 - Bubble trajectory
 - Bubble deformation
 - Vortex shedding in the bubble wake

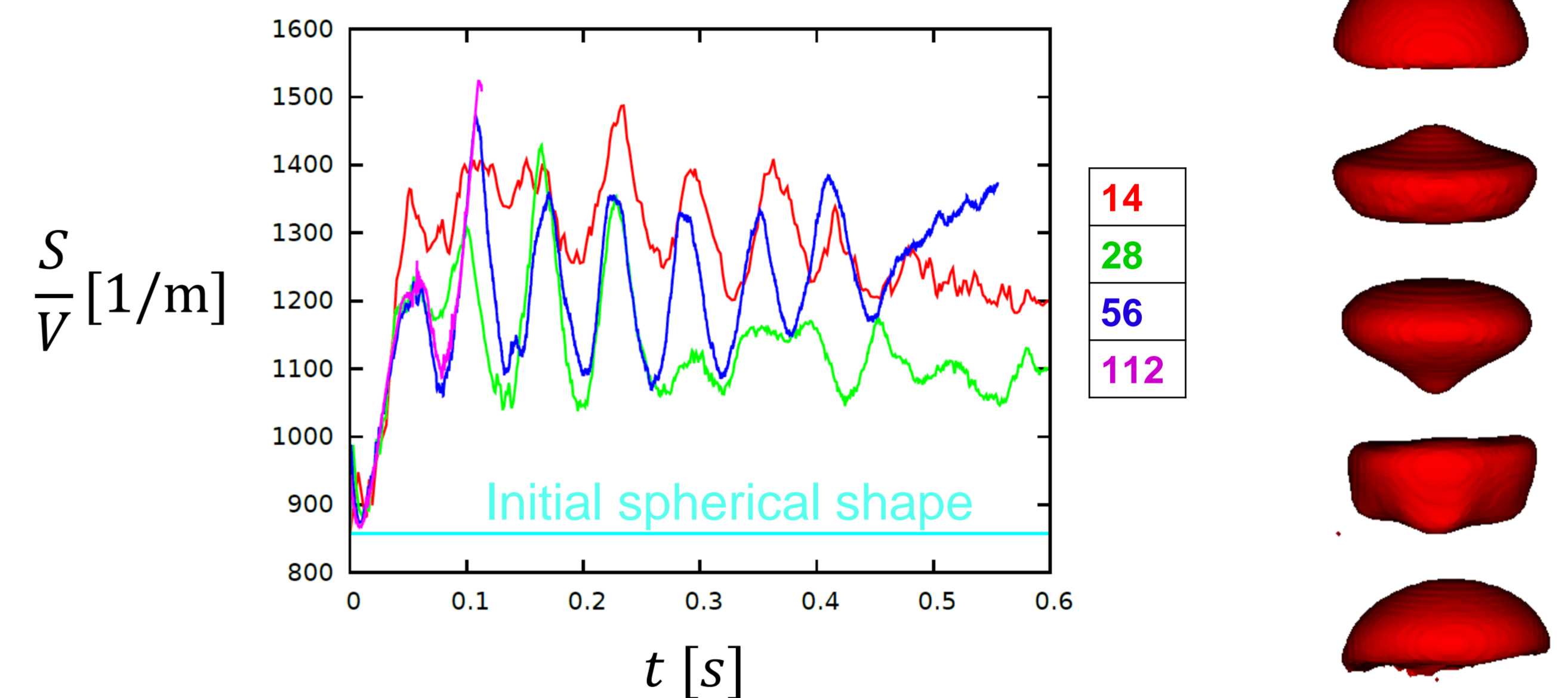


Fig. 1: Bubble shape oscillations evaluated by means of the surface-to-volume ratio; Including grid resolution sensitivity (colored numbers represent the number of cells per initial bubble diameter)

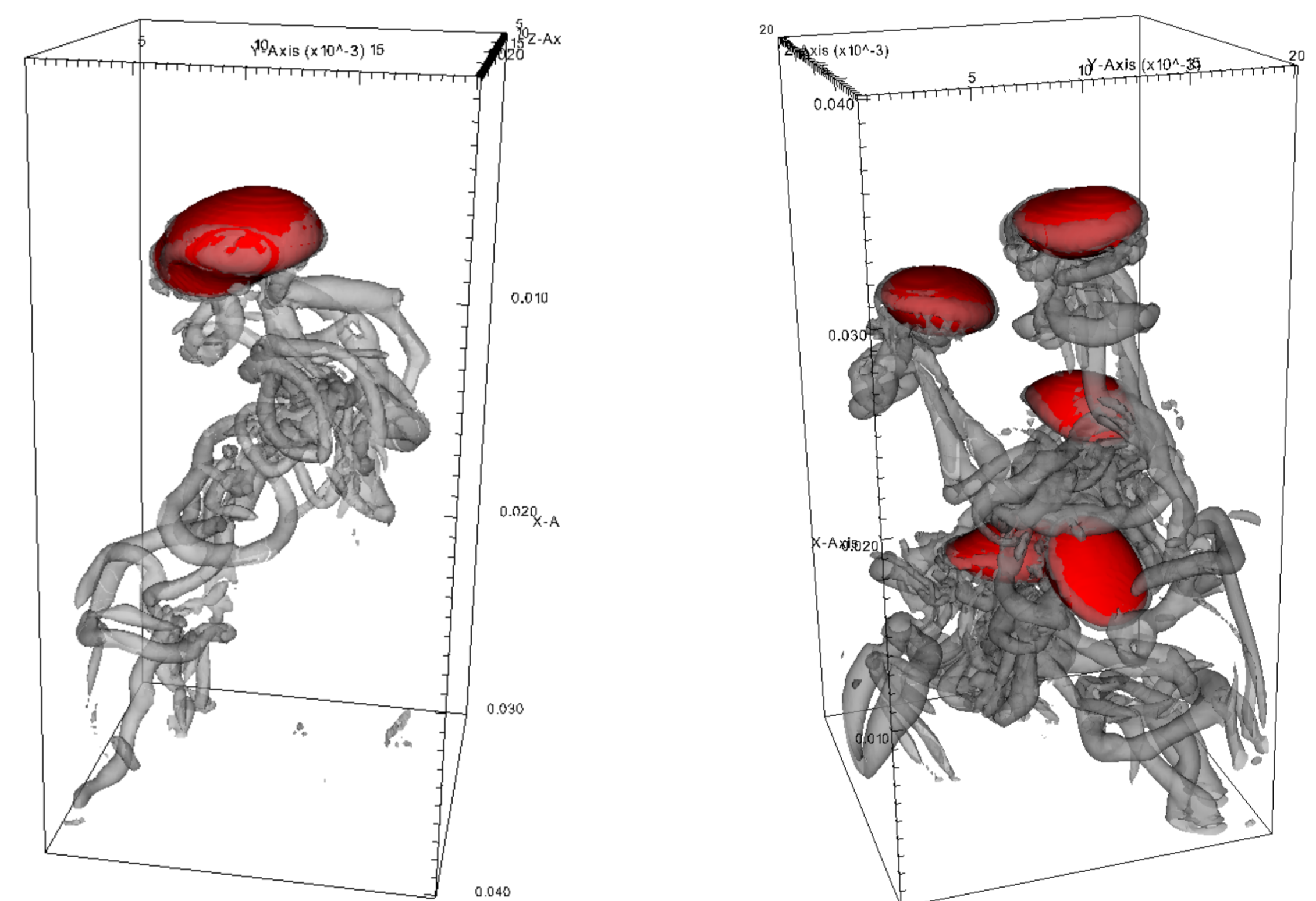


Fig. 2: Coherent structures visualized by the Q-criterion; Single bubble (1 x 7 mm) on the left, bubble cluster (5 x 5 mm) on the right

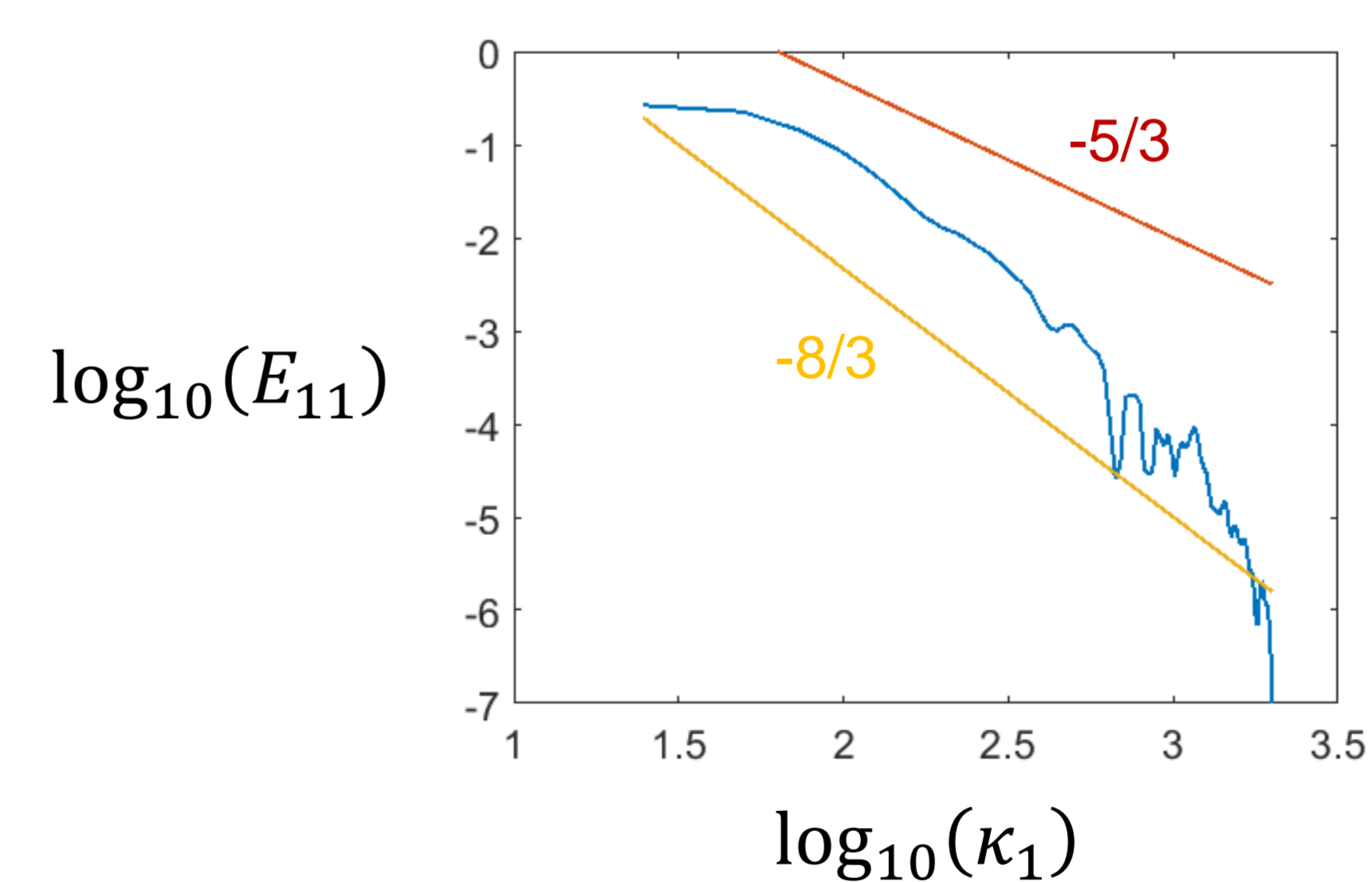


Fig. 3: Spatial energy spectrum in the bubble wake; Inertial sub-range -5/3 power law for single-phase turbulence and -8/3 for two-phase turbulence according to Lance & Bataille [5]

References

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